

**Form 4.1
Initial Data on the LP-Gas Facility**

A	B	C
Item #	Information Item	Data
1	Name of the LP-Gas Facility Owner or Operator	AmeriGas
2	Contact Name:	Thomas Green
3	Contact Telephone & Fax Numbers	(508) 693-5080 office (508) 693-0883 fax
4	Contact Email Address	thomas.green@amerigas.com
5	Mailing Address	Street 1: 6 North Line Road
		Street 2: Airport Industrial Park
		City, State, Zip: Edgartown, MA 02539

**Form 4.2
Facility Storage Capacity^{1,2,3}**

A	B	C	D
Item #	Individual Container Water Capacity (w.c.) (gallons)	Number of containers	Total Water Capacity (w.c.) of each container size (gallons)
1	500		
	1,000		
	2,000		
	4,000		
	10,000		
	18,000		
	30,000	4	120,000
	60,000		
	Other:		
	Other:		
Other:			
Other:			
2	Aggregate Water Capacity ⁴	4	120,000

- Notes:
- (1) Column D = Column B x Column C.
 - (2) Parked bobtails, transports and tank cars should not be considered for aggregate capacity calculations.
 - (3) Do not consider containers that are not connected for use.
 - (4) For the purpose of this manual, "Aggregate Water Capacity" means any group of single ASME storage containers separated from each other by distances less than those stated in the aboveground containers column of Table 6.3.1.

If the aggregate water capacity of the LP-Gas facility is less than or equal to 4,000 gallon (w.c.), no further assessment is required.

YOU CAN STOP HERE.

Form 4.3
Additional Information on the LP-Gas Facility

Existing Facility; Built to NFPA 58 Edition _____ Proposed Facility

a) Name of the Facility (if applicable) AmeriGas, Vineyard Propane

b) Type of LP-Gas Facility Commercial Industrial Bulk Plant

c) Facility is located in Rural Area, Suburban Area, City Commercial Zone
 City Industrial Zone

d) Facility neighbors[§]: Agri. fields Commercial Bldgs. Flammable Liquids Storage
(Check all that apply) Industrial Activity (metal fabrication, cutting and welding, etc)
 Manufacturing Others (explain) _____

e) Geographic Location of Facility/Address: 41.3946900, -70.6037366

f) Landmarks, if any: East of Martha's Vineyard Airport

g) LP-Gas liquid supply by: Bobtail Truck Transport Rail Tank Car
(Check all that apply) Pipeline

h) LP-Gas Distribution by: Bobtail Truck Transport Vapor Piping
(Check all that apply) Liquid Piping Dispensing or Vehicle Liquid fueling

i) Number of Vehicle Entrances: One Two More than two

j) Type of Access Roads to the Facility Rural City or Town Highway
(One check per line) Entrance 1 Dirt road Gravel road Paved
(One check per line) Entrance 2 Dirt road Gravel road Paved

k) Staff presence Not staffed Only during transfer operations
 Staffed always (24/7) Only during business hours
 Other (Explain) _____

l) Location and distances to Assembly, Educational or Institutional Occupancies surrounding the facility, if any, within 250 ft from the facility boundary in the direction of the assets.
None

m) Overview plot plan of the facility attached? Yes No

§ All properties either abutting the LP-Gas facility or within 250 feet of the container or transfer point nearest to facility boundary.

Form 5.4

Compliance with Code Requirements for Appurtenances on Containers Having a Water Capacity Greater Than 4,000 Gallons Used in Bulk Plants and Industrial Plants

A	B	C	D		E	F	G
Container #	LP-Gas inlet to and outlet from the container**		Enter Configuration Number		Total Number of Product Control Appurtenances		NFPA 58 Section Reference (2008 edition)
					Required by NFPA 58 (applicable edition)	Installed on the container	
1	Vapor	Inlet	5-2	3	2	3	See §5.7.4.2 and Table 5.7.4.2
		Outlet	5-3	2	2	3	
	Liquid	Inlet	5-6	2	2	3	
		Outlet	5-7	1	2	3	
2	Vapor	Inlet	5-2	3	2	3	
		Outlet	5-3	2	2	3	
	Liquid	Inlet	5-6	2	2	3	
		Outlet	5-7	1	2	3	
3	Vapor	Inlet	5-2	3	2	3	
		Outlet	5-3	2	2	3	
	Liquid	Inlet	5-6	2	2	3	
		Outlet	5-7	1	2	3	
4	Vapor	Inlet	5-2	3	2	3	
		Outlet	5-3	2	2	3	
	Liquid	Inlet	5-6	2	2	3	
		Outlet	5-7	1	2	3	

** If the container does not provide an opening for the specific function listed, enter 0 (zero) in columns E and F corresponding to that row.

If in Form 5.4 any one of the numbers in column F is less than the number in Column E of the corresponding row, these items must be addressed and brought into compliance with the specific edition of NFPA 58 that the facility was constructed to.

Form 5.5
Requirements for Transfer Lines of 1½-inch Diameter or Larger,
Liquid-into-Containers

A Item #	B Appurtenance (Either No. 1 or No. 2)**	C Appurtenance Provided with the Feature	D Installed in the facility?		E NFPA 58 Section Reference (2008 edition)
			Yes	No	
1	Emergency Shutoff Valve (ESV) (Ref § 6.12)	Installed within 20 ft. of lineal pipe from the nearest end of the hose or swivel-type connections.	✓		6.12.2
		Automatic shutoff through thermal (fire) actuation with melting point of thermal element < 250 °F	✓		6.12.6
		Temperature sensitive element (fusible link) installed within 5 ft from the nearest end of the hose or swivel type piping connected to liquid transfer line.	✓		6.12.6
		Manual shutoff feature provided at ESV installed location.	✓		6.12.10 (1)
		Manual shutoff device provided at a remote location, not less than 25 ft., and not more than 100 ft. from the ESV.	✓		6.12.10 (2)
		An ESV is installed on each leg of a multi leg piping each of which is connected to a hose or a swivel type connection on one side and to a header of size 1½ inch in diameter or larger on the other side.	✓		6.12.5 6.18.2.6 (1)
		Breakaway protection is provided such that in any pull-away break will occur on the hose or swivel-type connection side while retaining intact the valves and piping on the plant side.	✓		6.12.8
2	Back flow Check Valve (BCK)**	Installed downstream of the hose or swivel-type connection	✓		6.12.8
		BCK is designed for this specific application.	✓		6.12.4
		A BCK is installed on each leg of a multi leg piping each of which is connected to a hose or a swivel type connection on one side and to a header of 1½ inch in diameter or larger on the other side.	✓		6.12.5
		Breakaway protection is provided such that in any pull-away break will occur on the hose or swivel-type connection side while retaining intact the valves and piping on the plant side.	✓		6.12.8

** In lieu of an emergency shutoff valve, the backflow check valve (BCK) is only permitted when flow is only into the container and shall have a metal-to-metal seat or a primary resilient seat with metal backup, not hinged with a combustible material (6.12.3, 6.12.4).

Form 5.6
Requirements for Transfer Lines of 1½-inch Diameter or Larger,
Liquid Withdrawal From Containers

A Item #	B Appurtenance	C Appurtenance Provided with the Feature	D Installed in the facility?		E NFPA 58 Section Reference (2008 Edition)
			Yes	No	
1	Emergency Shutoff Valve (ESV) (Ref § 6.12.1)	Installed within 20 ft. of lineal pipe from the nearest end of the hose or swivel-type connections.	✓		6.12.2
		Automatic shutoff through thermal (fire) actuation with melting point of thermal element < 250 °F.	✓		6.12.6
		Temperature sensitive element installed within 5 ft from the nearest end of the hose or swivel type piping connected to liquid transfer line.	✓		6.12.6
		Manual shutoff feature provided at ESV installed location.	✓		6.12.10 (1)
		Manual shutoff device provided at a remote location, not less than 25 ft., and not more than 100 ft. from the ESV.	✓		6.12.10 (2)
		An ESV is installed on each leg of a multi leg piping each of which is connected to a hose or a swivel type connection on one side and to a header of 1½ inch in diameter or larger on the other side.	✓		6.12.5 6.18.2.6 (1)
		Breakaway protection is provided such that in any pull-away break will occur on the hose or swivel-type connection side while retaining intact the valves and piping on the plant side.	✓		6.12.8
		Number of ESV's in liquid withdrawal service			1

Note: If more than one ESV is installed in the facility, use one Form 5.6 for each ESV.

Form 5.7
Requirements for Vapor Transfer Lines 1¼-inch Diameter or Larger

A Item #	B Appurtenance	C Appurtenance Provided with the Feature	D Installed in the facility?		E NFPA 58 Section Reference (2008 edition)
			Yes	No	
1	Emergency Shutoff Valve (ESV) (Ref § 6.12.1)	Installed within 20 ft. of lineal pipe from the nearest end of the hose or swivel-type connections.	X		6.12.2
		Automatic shutoff through thermal (fire) actuation with melting point of thermal element < 250 °F	X		6.12.6
		Temperature sensitive element installed within 5 ft from the nearest end of the hose or swivel type piping connected to liquid transfer line.	X		6.12.6
		Manual shutoff feature provided at ESV installed location.	X		6.12.10 (1)
		Manual shutoff device provided at a remote location, not less than 25 ft., and not more than 100 ft. from the ESV.	X		6.12.10 (2)
		An ESV is installed on each leg of a multi leg piping each of which is connected to a hose or a swivel type connection on one side and to a header of 1-1/4 inch in diameter or larger on the other side.	X		6.12.5 6.18.2.6 (1)
		Breakaway protection is provided such that in any pull-away break will occur on the hose or swivel-type connection side while retaining intact the valves and piping on the plant side.	X		6.12.8
2	Back flow Check Valve (BCK)**	Installed downstream of the hose or swivel-type connection	X		6.12.8
		BCK is designed for this specific application.	X		6.12.3 and 6.12.4
		A BCK is installed on each leg of a multi leg piping each of which is connected to a hose or a swivel type connection on one side and to a header of 1-1/4 inch in diameter or larger on the other side.	X		6.12.5
		Breakaway protection is provided such that in any pull-away break will occur on the hose or swivel-type connection side while retaining intact the valves and piping on the plant side.	X		6.12.8

** In lieu of an emergency shutoff valve, the backflow check valve (BCK) is only permitted when flow is only into the container and it shall have a metal-to-metal seat or a primary resilient seat with metal backup, not hinged with a combustible material (6.12.3, 6.12.4).

If a checkmark is made in the "No" column of any one of Form 5.5, Form 5.6 or Form 5.7, then these items must be addressed and brought into compliance with the specific edition of NFPA 58 that the facility was constructed to.

If the LP-Gas facility is designed using ALTERNATE PROVISIONS for the installation of ASME CONTAINERS, then continue the analysis below. Otherwise skip Forms 5.8 and 5.9 and go to Chapter 6.

Form 5.8 Evaluation of Redundant Fail-Safe Design

A	B		C	D	E	F
I t e m #	Description		Features	Installed in the facility?		NFPA 58 Section Reference (2008 edition)
				Yes	No	
1	Container Sizes for which the appurtenances are provided		Appurtenances and Redundant Fail-Safe equipment are provided for <u>each</u> container of water capacity 2,001 gal. through 30,000 gal.	X		6.26.3 and 6.26.4
2	Liquid or Vapor withdrawal (1-1/4 in. or larger)		Internal Valve with integral excess flow valve or excess flow protection	X		6.26.3.1
			Positive Shutoff Valve installed as close as practical to the Internal Valve	X		6.26.3.4
3	Liquid or Vapor Inlet		Internal Valve with integral excess flow valve or excess flow protection or Back Flow Check valve	X		6.26.3.5
			Positive Shutoff Valve installed as close as possible to the Internal Valve or the back flow check valve	X		6.26.3.5
4	Railcar Transfer	Flow Into or Out of Railroad tank car	Approved emergency shutoff valves installed in the transfer hose or the swivel-type piping at the tank car end	NA	NA	6.18.2.6 (1) and 6.26.4.1
		Flow Only into railroad tank car	Approved emergency shutoff valve or backflow check valve installed in the transfer hose or the swivel-type piping at the tank car end	NA	NA	6.18.2.6 (2) and 6.26.4.1
5	Cargo Tank Transfer		Protection provided in accordance with 6.26.4.1	NA	NA	6.26.4.1
6	Automatic closure of all primary valves (IV & ESV) in an Emergency		Actuated by Fire Detection	NA	NA	6.26.4.2
			Actuated by a hose pull-away due to vehicle motion	X		6.26.4.2
7	Manually operated remote shutdown of IV and ESV		Remote shutdown station within 15 ft of the point of transfer?	X		6.26.4.3 (A)
			Another remote shutdown station between 25 ft and 100 ft of the transfer point?	X		6.26.4.3 (B)
			Shutdown stations will shut down electrical power supply, if any, to the transfer equipment and primary valves?		X	6.26.4.3
			Signs complying with the requirements of 6.24.4.3 (C) provided?	X		6.26.4.3 (C)

Note: If the facility does not have a rail terminal, write the word NA in both the "Yes" column and the "No" column in item 4 of this Form in the railroad tank car row. Similar option is also available if there is no cargo tank vehicle transfer station.

Form 6.1
Evaluation of Physical Protection and Other Measures

A	B	C	D	E	F
#	Item	Features	Installed in the facility?		NFPA 58 Section Reference (2008 Edition)
			Yes	No	
1	Lighting [‡]	Provide lighting for nighttime operations to illuminate storage containers, container being loaded, control valves, and other equipment	X		6.18.5
2	Vehicle impact protection	Protection against vehicular (traffic) impacts on containers, transfer piping and other appurtenances is designed and provided commensurate with the size of vehicles and type of traffic in the facility. (Example protection systems include but not limited to (1) Guard rails, (2) Steel bollards or crash posts, (3) Raised sidewalks.	X		6.9.3.10 and 6.19.3.2
3	Protection against corrosion	Provide protection against corrosion where piping is in contact with supports or corrosion causing substances.	X		6.9.3.11
Complete only 4A or 4B					
4A	Perimeter Fence	Is an industrial type or chain link fence of at least 6 ft high or equivalent protection provided to enclose (all around) container appurtenances, pumping equipment, loading and unloading and container filling facilities?	X		6.18.4.2
		Are at least two means of emergency accesses (gates) from the enclosure provided? NOTE: Write "N.A." (not applicable) if (i) The area enclosed is less than 100 ft ² , or (ii) The point of transfer is within 3 ft of the gate, or containers are not filled within the enclosure	X		6.18.4.2 (A)
		Is a clearance of at least 3 feet all around to allow emergency access to the required means of egress been provided?	X		6.18.4.2 (B)
	Guard Service	If a guard service is provided, does this service cover the LP-Gas plant and are the guard personnel provided with appropriate LP-Gas related training, per section 4.4 of NFPA 58?	NA	NA	6.18.4.3
4B	Lock-in-Place devices	Are Lock-in-Place devices provided to prevent unauthorized use or operation of any container appurtenance, system valves, or equipment in lieu of the fence requirements above?			6.18.4.2 (C)

Note: Fill only items 1, 2, 3, and 4A or 4B. Indicate with "NA" when not filling the "Yes" or "No" column.

[‡] Indicate with "NA" if the facility is not operated at night.

Form 6.2

Assessment of Sources of Ignition and Adjacent Combustible Materials

A	B	C	D	E
#	Sources of Ignition and Requirements Pertaining to Adjacent Combustible Materials	Is the Facility compliant?		NFPA 58 Section Reference (2008 Edition)
		Yes	No	
1	Are combustible materials, weeds and tall grass not closer than 10 ft. from each container?	X		6.4.5.2
2	Is a distance at least 20 ft. provided between containers and tanks containing flammable liquids with flash point less than 200 °F (ex., gasoline, diesel)?	X		6.4.5.5
3	Are electrical equipment and wiring installed per Code requirements?	X		6.22.2
4	Is open flame equipment located and used according to Code?	X		6.22.3.1
5	Are ignition control procedures and requirements during liquid transfer operations complied with.?	X		7.2.3.2
6	Is an approved, portable, dry chemical fire extinguisher of minimum capacity 18 Lbs. and having a B:C rating provided in the facility?	X		6.25.4.2
7	Is an approved, portable, dry chemical fire extinguisher of minimum capacity 18 Lbs. and having a B:C rating provided on each truck or trailer used to transport portable containers?	X		9.4.7
8	Is the prohibition on smoking within the facility premises strictly enforced?	X		7.2.3.2 (B) & 9.4.10

Note: Insert "NA" in both "Yes" and "No" columns of any items that are not applicable.

Form 6.3

Separation Distances from Containers to Buildings, Property Lines that can be Built upon, Inter-container Distances, and Aboveground Flammable or Combustible Storage Tanks

A #	B Container Size Range in gal (W.C.)	C Separation between a property line, important building or other property and the <u>nearest</u> container which is	D Minimum Distance (ft)	E Is the Facility compliant?		G NFPA 58 Section Reference (2008 Edition)
				Yes	No	
1	501 through 2,000	Above Ground	25	NA	NA	6.3.1 and Table 6.3.1
		Underground or Mounded	10	NA	NA	
		Between containers	3	NA	NA	
2	2,001 through 30,000	Above Ground	50	X		
		Underground or Mounded	50	NA	NA	
		Between containers	5	X		
3	30,001 through 70,000	Above Ground	75	NA	NA	
		Underground or Mounded	50	NA	NA	
		Between containers	¼ sum of diameters of adjacent containers	NA	NA	
4	70,001 through 90,000	Above Ground	100	NA	NA	
		Underground or Mounded	50	NA	NA	
		Between containers	¼ sum of diameters of adjacent containers	NA	NA	
5	All sizes greater than 125 gal	Separation distance between a LP-Gas container and an above ground storage tank containing flammable or combustible liquids of flash points below 200 °F.	20	NA	NA	6.4.5.4 and 6.4.5.5

Note: If any of the container sizes indicated in the above form are not present in the facility, enter "NA" in both Yes and No columns.

If the LP-Gas plant is provided with every one of the redundant and fail-safe product control-design equipment indicated in Form 5.8, then the minimum distance in column D of Form 6.3 can be reduced to 10 feet for underground and mounded containers of water capacity 2,001 gal to 30,000 gal.

Form 6.4

Separation Distances between Points of Transfer and other Exposures

A	B		C	D	E		F	G
#	Type of Exposure within or outside the facility boundary		Check if exposure is present	Minimum Distance (ft)	Is the Facility compliant?			NFPA 58 Section Reference (2008 Edition)
					Yes	No		
1	Buildings, mobile homes, recreational vehicles, and modular homes with fire-resistive walls			10	NA	NA		Section 6.5.3 Table 6.5.3
2	Buildings with other than fire resistive walls		X	25	X			
3	Building wall openings or pits at or below the level of the point of transfer			25	NA	NA		
4	Line of adjoining property that can be built upon		X	25	X			
5	Outdoor places of public assembly, including school yards, athletic fields, and playgrounds			50	NA	NA		
6	Public ways, including public streets, highways, thoroughfares, and sidewalks	From points of transfer in LP-Gas dispensing stations and at vehicle fuel dispensers.	X	10	X			
		From other points of transfer	X	25	X			
7	Driveways		X	5	X			
8	Mainline railroad track centerlines			25	NA	NA		
9	Containers other than those being filled		X	10	X			
10	Flammable and Class II combustible liquid dispensers and aboveground and underground containers			20	NA	NA		
11	Flammable and Class II combustible liquid dispensers and the fill connections of LPG containers			10	NA	NA		
12	LP-Gas dispensing device located close to a Class I liquid dispensing device.			10	NA	NA	6.24.4.3	

NOTE: Place a checkmark in column C against an exposure that is present in or around the facility. Fill columns E or F for only those rows for which there is a checkmark in column C.

If the facility contains low emission transfer equipment (i.e, all equipment identified in Form 5.9 are installed and are in working order), then the minimum separation distances in column D of Form 6.4 can be reduced to one half of the indicated values.

If the containers in the LP-Gas facility are provided with SPECIAL PROTECTION MEASURES, then continue the analysis below. Otherwise skip Forms 6.5 and 6.6 and go to Form 6.7. Also see Chapter 9.

Form 6.7
Protection Against Vehicular Impact

#	System Protected	Is physical protection provided?		Type of physical protection installed
		Yes	No	
1	Storage containers	X		Concrete Barriers
2	Transfer stations	X		Concrete Barriers
3	Entryway into plant	X		Gate

Table 7.1
Distances to Various Types of Propane Hazards Under Different Release Models**

Model #	Details of the Propane Release Model Releases from or due to	Vapor Dispersion Distance to LFL (ft)	Explosion Hazard Distance (ft)	Fire Ball Radiation Distance (ft)	
1A	Bobtail hose failure. Release of the entire inventory in the hose, quickly.	1" ID x 150 ft hose length	250	110	50
1B		1" ID x 120 ft hose length	230	103	45
1C		1" ID x 75 ft hose length	190	90	40
2a	Release of the inventory in a transfer piping 1" x 30 ft + @ 20 gpm for 10 min., due to failed excess flow valve.	135	120	25	
2b	Release of the inventory in a transfer piping 2" x 30 ft + @80 gpm for 10 mins.	230	252	48	
2c	Release of the inventory in a transfer piping 2" x 80 ft. @ 70 gpm for 10 mins.	328	235	74	
2d	Release of the inventory in a transfer piping 2.5" x 30 ft @80 gpm for 10 mins.	269	252	59	
2e	Release of the inventory in a transfer piping 3" x 30 ft + @100 gpm for 10 mins.	312	287	69	
2f	Release of the inventory in a transfer piping 3" x 18 ft + @100 gpm for 10 mins.	256	284	55	
3	Release from the container pressure relief valve	No ignitable vapor concentration at ground level			
4	Release from a 1" ID x 150 ft transfer piping to a vaporizer and reduced flow from a partially open excess flow valve @ 20 gpm for 10 min.	250	120	50	
5	Leak from a corrosion hole in a transfer pipe at a back pressure of 130 psig (corresponding to 80 °F) for 60 min. Hole size is ¼" ID.	110	120	5	
6	Release of the entire inventory in a 2" ID x 20 ft., transfer hose.	195	90	40	
6a	Release of the entire inventory in a 2.5 inch dia. transfer hose x 16 ft. length	215	98	45	
6b	Release of the entire inventory in a 3-inch dia. transfer hose x 12 ft. length	230	100	46	
7	Transport hose blow down: Hose size 2" ID, 20 ft length release for 3min., from a Transport after the tank is filled.	25	30	<5	
7a	Transport hose blow down: Hose size 2.5" ID, 16 ft length release for 3min., from a Transport after the tank is filled.	25	29	<5	
7b	Transport hose blow down: Hose size 3" ID, 16 ft length release for 3min., from a Transport after the tank is filled.	31	36	<5	

** Results from models described in Appendix B. The results are rounded to the nearest 5 feet.

Form 7.1
Types of Occupancies⁽¹⁾ Near or Surrounding the LP-Gas Facility

Type of Occupancies	Model # from Table 7.1	Hazard Distance ⁽²⁾ (feet)	Is Occupancy located within the hazard distance from the Facility?	
			Yes	No
Assembly Occupancies (Places of worship, Libraries, Theaters and Auditoriums, Food or Drink Bars, Sports Stadiums, Amusement Parks, Transportation Centers, etc. with 50 or more people).	NA	NA		X
Institutional Occupancies (Elderly Persons Home or Nursing Home, Hospitals, Alcohol & Drug Rehabilitation Centers, Prisons)	NA	NA		X
Educational Occupancies (Elementary Schools, Day Care facilities, etc).	NA	NA		X

NOTES: (1) Different types of occupancies are defined in NFPA 5000

(2) Table 7.1 provides a number of scenarios that can result in propane release, and the resulting area exposed for different ignition mechanisms. Determine the scenarios that are applicable to the facility, for the quantities that can be released, and enter the greatest value from Table 7.1. Use the hose diameters and length that will be used at the facility if they differ from the ones in Table 7.1 and recalculate the hazard distances using a spreadsheet method that is available at npga.org. Some scenarios may not be applicable to an installation because of other mitigation measures implemented, such as a hose management procedure to minimize the possibility of hose failure.

Form 7.2
Exposure to LP-Gas Facility from External Hazards

A	B	C	D
Item #	Type of Neighboring Operation	Hazard exists to the LP-Gas Facility	
		Yes	No
1	Petroleum and other hazardous material storage, wholesale dispensing, etc.		X
2	Metal cutting, welding, and metal fabrication		X
3	Industrial Manufacturing that can pose external hazards		X
4	Ports, rail yards and trans-shipment terminals handling flammable and explosive materials.		X
5	Other operations that may pose hazards (gasoline and other hazardous material dispensing stations, fertilizer storage, etc).		X

NOTE: If a particular activity indicated in column B does not exist, fill both "Yes" and "No" columns with "NA."

Where a "Yes" has been checked in either Form 7.1 or Form 7.2:

- 1) For an existing facility, communicate this information to local emergency responders for inclusion in their emergency planning.
- 2) For a proposed facility, implement the actions indicated in Chapter 9.

Form 8.1
Data on the Responding Fire Department

A	B		C
Item #	<u>Data Item</u>		Data Entry
1	Name of the Fire Department (FD).		Edgartown
2A	Name of the person in the FD assisting with the data acquisition.		Alex Schaeffer
2B	Position of the person in the FD assisting with the data acquisition.		Fire Chief
3A	Date on which FD data was collected.		1-22-21
3B	Name of the person collecting the data.		Alex Schaeffer
4	Number of firefighters on duty at any time.		3-4
5	Average number of firefighters available for response.		4-10
6A	Number of firefighters qualified to	“Firefighter I” level.	11
6B		“Firefighter II” level.	18
7A	Number of firefighters who would:	Respond on the first alarm to the facility.	4
7B		Respond on the first alarm and who are qualified to the operations level requirements of NFPA 472 or <u>similar</u> local requirements	4
7C		Respond on the first alarm with specific knowledge and training on the properties of LP-Gas and LP-Gas fires.	1
8A	Number of fire apparatus that have the capability to deploy a 125 gpm hose line supplied by onboard water for at least 4 minutes, and, which:	Are in service in the department.	4
8B		Would respond on a first alarm.	1-3

Form 8.2
Response Time data for the Fire Departments

A	B	C	D	E
Company or Department	Time in Minutes for			
	Alarm Receipt & Handling	Turnout	Travel	Total Time
Edgartown Fire Dept.	Dukes county safety office	3 min day/5-10 night	8-10	11-13 day/15-20 night

Note: Number in Column E = Sum of numbers from Columns B through D.

Form 8.3

Water Flow Rate and Total Water Volume Required to Cool Containers Exposed to a Fire

A	B	C	D	E	F	G	H
Item #	ASME Container Size (gallons)	Total Surface Area of each Container ¹ (ft ²)	Surface Area of each container to be Cooled (ft ²)	Water flow rate required per container (gpm)	Number of containers of the size indicated ‡	Total Water flow rate required (gpm)	Total volume of water required for 10 min (gal)
1	500	86	43	10.8			
	1,000	172	86	21.5			
	2,000	290	145	36.3			
	4,000	374	187	46.8			
	6,500	570	285	71.3			
	9,200	790	395	98.8			
	12,000	990	495	123.8			
	18,000	1,160	580	145.0			
	30,000	1,610	805	201.3	4	805.2	
	45,000	2,366	1,183	295.8			
	60,000	3,090	1,545	386.3			
	90,000	4,600	2,300	575.0			
	Other Size						
2a	Calculated water flow rate for container protection					805.2	
2b	Water flow rate rounded up to nearest multiple of 125					900	
3	Water for firefighter protection, if required					250	
4	Total water flow rate and volume					1150	

Note: Column D = (1/2) x Column C
 Column E = 0.25 (gpm/ft²) x Column D ;
 Column G = Column F x Column E
 Column H = 10 x Column G
 Line 2a, Column G and Column H are the sum of numbers in each row above line 2 of each column.
 Line 4, Column G and Column H are the sum of numbers in rows 2b and 3.

‡ Consider only 3 containers for water supply evaluations even if the number of containers in a group is more than 3. See Section 8.2.

1 ASME container approximate dimensions

The total water requirement for the facility is indicated in item 4, column G (water flow rate) and column H (total water volume or quantity) of Form 8.3. If multiple groups of containers are present in the facility, repeat the calculations in Form 8.3 for each group of containers. The total water requirement for the facility is the largest value for any single group of containers.

Form 8.4
Evaluation of Water Availability in or Near the LP-Gas Facility

A	B	C	D		
Item #	Water from...	Available?	Quantitative information		
1	Public supply or from another piped-in supply through one or more fire hydrants in or near the facility	<input checked="" type="checkbox"/> Yes <input type="checkbox"/> No	Hydrant data	Distance from Container(s) on which water will be applied (feet)	Available water flow rate from all hydrants ⁽¹⁾ (gpm)
			Hydrant 1	322	
			Hydrant 2	NA	
			Hydrant 3	NA	
2	A nearby static water source (stream, pond, lake, etc).	<input type="checkbox"/> Yes <input checked="" type="checkbox"/> No	Distance to water source = _____ Feet Time to set up relay = _____ min. Rate of delivery = _____ gpm		
3	Only through mobile water tanker shuttle.	<input type="checkbox"/> Yes <input checked="" type="checkbox"/> No	Time to set up shuttle = _____ min. Sustainable flow rate = _____ gpm		

(1) Obtain the available flow rate from the local municipal water authority or the entity that supplies water to the hydrant or conduct a test to determine total available flow rate.

- 1. For an existing facility, communicate this information to local responders for inclusion in their emergency planning.**
- 2. For a proposed new facility, refer to Chapter 9**

Form 9.1

Analysis Summary on Product Control and Local Conditions of Hazard

A	B	C	D	E
Item #	CHAPTER Title	Section & Title	Reference FORM #	Number of "No" checked
1	Product Control Measures in Containers & Transfer Piping	5.1: Product Control in Containers	5.1 or 5.2 or 5.3 or 5.4 [§]	0
		5.2 Product Control in Transfer Piping	5.5	0
			5.6	0
			5.7	0
			5.8	0
			5.9	0
2	Analysis of Local Conditions of Hazard	6.1 Physical Protection Measures	6.1	0
		6.2 Ignition Source Control	6.2	0
		6.3.1 Separation distances; Container and outside exposures	6.3	0
		6.3.2 Separation distances; Transfer points and outside exposures	6.4	0
		6.4 Special Protection Measures	6.5	0
			6.6	0

§ The number of "No" for Forms from Chapter 5 is the difference between the required number of appurtenances according to NFPA 58-2008, and a lesser number found to be actually installed on the container or the transfer piping.

If, in any row of column E ("No") of Form 9.1, the entry number is greater than zero, the proposed LP-Gas facility is not in compliance with the requirements of NFPA 58-2008 for product control appurtenances or other safety measures. The design of the proposed facility must be modified to conform to the Code requirements. In addition, the following items should be noted.

- If there are any "No" checks in Form 6.3, then the separation distance requirements for containers are not satisfied. An option that may be considered is the reduction in separation distance to 10 feet for underground and mounded containers by providing "Redundant and Fail-Safe Product Control Measures." In this case, complete Form 9.4 below to ensure that each requirement of "Redundant and Fail-Safe Product Control Measures" is provided.
- If there are any "No" checks in Form 6.4, then the separation distance requirements for transfer points are not satisfied. In this case, relocate the transfer points so that the separation distances conform to the code requirements or provide the Low Emission Transfer Equipment. Complete Form 9.5 below and ensure that all requirements for Low Emission Transfer Equipment are fulfilled.

Form 9.2
Analysis Summary on Exposure from and to the LP-Gas Facility

A	B	C	D	E
Item #	CHAPTER Title	Section & Title	Reference FORM #	Number of "Yes" checked
1	Exposure to and from Other Properties	7.1 Exposure to off-site properties and persons from in-plant propane releases	7.1	0
		7.2 Exposure to propane facility from external events.	7.2	0

If the entry number in column E ("Yes"), Form 9.2 corresponding to Form 7.1 is greater than zero, consider one or more of the following design alternatives.

- 1 Consider moving the container or the transfer point to a different location, if possible and space exists, so that the property or the person is beyond the hazard distance.
- 2 Provide "Redundant and Fail-safe Product Control Measures". Complete Form 9.4 to ensure compliance.
- 3 Institute other technical measures such as installing gas and flame detectors (connected to facility shut down systems), sounding alarm outside facility premises, etc.
- 4 Institute administrative controls such as additional training for personnel, more frequent inspections of hoses and transfer piping, etc.

If the entry number in column E ("Yes"), Form 9.2 corresponding to Form 7.2 is greater than zero, consider one or more of the following design alternatives.

- 1 Implement procedures to monitor neighboring activity.
- 2 Install means in the adjacent plant to shut down the LP-Gas plant in case of an emergency in that plant.

Form 9.3
Analysis Summary on Fire Department Evaluations

A	B	C	D	E	F
Item #	CHAPTER Title	Section & Title	Reference FORM #	Number "zeros" entered in Column C, Lines 6 through 8 of Form 8.1	Number of "Yes" checked in Column C of Form 8.4
1	Fire department capability, adequacy of water supply and Emergency Planning	8.1 Data on the Fire Department	8.1	0	
2		8.2 Fire response water needs and availability	8.4		1

If the entry number in row 1, Column E of Form 9.3 is greater than zero, consider one or more of the following design alternatives.

- 1 Discuss with the local Fire Department the needs of the LP-Gas facility and the evaluation results on the capability and training inadequacies of the Department.
- 2 Consider developing a cadre of personnel within the LP-Gas facility to respond to emergencies.
- 3 Institute container special protection system based on active protection approaches or passive approaches. Complete Form 9.6 and Form 9.7 below.

If the entry number in row 2, Column F of Form 9.3 is equal to zero, consider one or more of the following design alternatives.

- 1 Provide special protection (other than water spray or monitor systems) to containers, satisfying the requirements of section 6.23.5 of NFPA 58, 2008 edition. Complete Form 9.6 to ensure compliance.

Consider implementing the various options indicated in Table 9.1.

Form 9.4
Redundant and Fail-Safe Design for Containers

A Item #	B Description		C Features	D Proposed for the facility?		F NFPA 58 Section Reference (2008 Edition)
				Yes	No	
1	Container Sizes for which the appurtenances are provided		Appurtenances and redundant fail-safe equipment and Low Emission transfer lines are provided for <u>each</u> container of water capacity 2,001 gal to 30,000 gal	X		6.26.4 and 6.26.5
2	Liquid or Vapor Withdrawal (1-1/4 in. or larger)		Internal Valve with integral excess flow valve or excess flow protection	X		6.26.3.1
			Positive Shutoff Valve installed as close as possible to the Internal Valve	X		6.26.3.4
3	Liquid or Vapor Inlet		Internal Valve with integral excess flow valve or excess flow protection or Back Flow Check valve	X		6.26.3.5
			Positive Shutoff Valve installed as close as possible to the Internal Valve or the back flow check valve	X		6.26.3.5
4	Railcar Transfer	Flow Into or Out of Railroad tank car	Emergency shutoff valve installed in the transfer hose or the swivel-type piping at the tank car end.	NA	NA	6.18.2.6 (1) and 6.26.4.1
		Flow Only Into railroad tank car	Emergency shutoff valve or backflow check valve installed in the transfer hose or the swivel-type piping at the tank car end.	NA	NA	6.18.2.6 (2) and 6.26.4.1
5	Cargo Tank Transfer		Protection provided in accordance with 6.26.4.1	NA	NA	6.26.4.1
6	Automatic closure of all primary valves (IV & ESV) in an Emergency		By fire actuation	X		6.26.4.2
			In the event of a hose pull-away due to vehicle motion	X		6.26.4.2
7	Manually operated remote shutdown of IV and ESV		Remote shutdown station within 15 ft of the point of transfer?	X		6.26.4.3 (A)
			Another remote shutdown station between 25 ft and 100 ft of the transfer point?	X		6.26.4.3 (B)
			Shutdown stations will shut down electrical power supply, if any, to the transfer equipment and primary valves?		X	6.26.4.3
			Signs complying with the requirements of 6.24.4.3 (C) provided?	X		6.26.4.3 (C)

Note: If your facility does not have a rail terminal, write the word NA in both the "Yes" column and the "No" column in item 4 of the form in the railroad tank car row. Similar option is also available if there is no cargo tank vehicle transfer station.

Form 9.5
Evaluation of Low Emission Transfer Equipment

A Item #	B Description	C Features		D Proposed for the facility?		F NFPA 58 Section Reference (2008 Edition)
				Yes	No	
1	Transfer into Cylinders or ASME Containers on Vehicles	Delivery Nozzle and Filler Valve- Max. Liquid Release after transfer of 4 cc.	Fixed Maximum Liquid Level Gauge not used during transfer operations	NA	NA	6.26.5.1 (B)
2	Transfer into Stationary ASME Containers Delivery valve and nozzle combination	During product transfer or post transfer uncoupling of the hose, liquid product volume released to the atmosphere	Does not exceed 4 cc (0.24 in ³) from a hose of nominal size 1 in or smaller	NA	NA	6.26.5.1 (A)
			Does not exceed 15 cc (0.91 in ³) from a hose of nominal size larger than 1 in.	NA	NA	6.26.5.2 (B)
3	Transfer into Stationary ASME Containers Maximum filling limit	Do containers less than 2,001 gal (w.c.) have an overfilling prevention device or another approved device?		NA	NA	6.26.5.2 (F)
		Do containers greater than 2,000 gal (w.c.) have a float gage or other non-venting device?		NA	NA	6.26.5.2 (E)
4	Transfer into Stationary ASME Containers Fixed Maximum Liquid Level gauge	Not used during routine transfer operations but may be used in calibrating other non-venting liquid level gauges in the container		NA	NA	6.26.5.2 (C,D)

Note: If the facility does not have a particular feature described in the table, write "NA" in both the "Yes" and "No" columns corresponding its row in item 2.

Form 9.6
Special Protection Measures –Passive Systems

A Item #	B Special Protection Option	C Question	D Proposed for the facility?		E NFPA 58 Section Reference (2008 Edition)
			Yes	No	
1	Container Insulation	Insulation provided on each of the containers?		X	6.25.5.1
		Insulation material complies with the requirements of section 6.25.5.1 of NFPA 58?	NA	NA	6.25.5.1 and 6.25.5.2
2	Mounding of containers	Each container in the facility is mounded?		X	6.25.5.3
		Mounding complies with each requirement under section 6.6.6.3 of NFPA 58.	NA	NA	6.25.5.3
3	Burying of containers	Each container in the facility is buried?		X	6.25.5.4
		Buried containers comply with each requirement under section 6.6.6.1 of NFPA 58.	NA	NA	6.6.6.1 & 6.25.5.4

Form 9.7
Special Protection Measures –Active Systems

Item #	Special Protection Option	Question	Is the Facility compliant?		NFPA 58 Section Reference (2008 Edition)
			Yes	No	
1	Water spray systems	Are fixed water spray systems, complying with NFPA 15 requirements, used for each container in the facility?	NA	NA	6.25.6.1
		Do fire responsive devices actuate water spray system automatically?	NA	NA	6.25.6.2
		Can the water spray systems be actuated manually also?	NA	NA	6.25.6.2
2	Monitor nozzle systems	Are the monitor nozzles located and arranged so that the water stream can wet the surfaces of all containers exposed to a fire?	NA	NA	6.25.6.3
		Can the water stream from a monitor nozzle reach and wet the entire surface of, at least, one half of a length from one end of each of the containers it is designed to protect?	NA	NA	6.25.6.3
		Do fixed monitor nozzles comply with NFPA 15 requirements?	NA	NA	6.25.6.1
		Do fire responsive devices actuate the monitor nozzles?	NA	NA	6.25.6.2
		Can the monitor nozzles be actuated manually also?	NA	NA	6.25.6.2

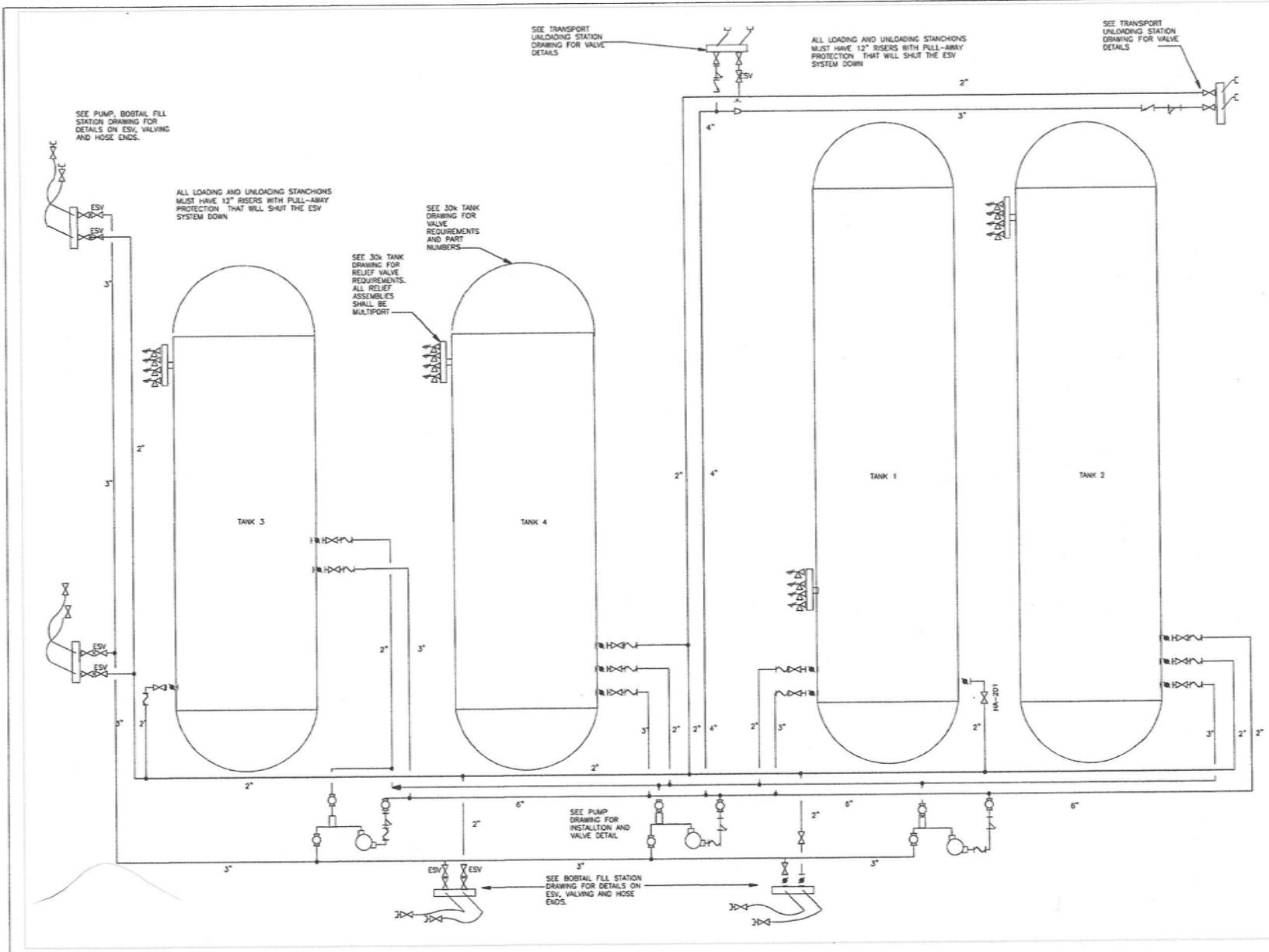
Equivalent Protection to a Water Supply for Industrial and Bulk Facilities

In the case where water supply is not available in or near the LP-Gas facility, or is inadequate or it is prohibitively expensive to connect to a public or private water supply hydrant, alternative methods for providing protection should be considered. In lieu of providing a water supply, several alternatives are indicated in Table 9.1, which can offer an equivalency to a water supply system.

The intent of the controls identified in Table 9.1 is to maintain the entire system as a gas tight entity. These methods include reducing the service life of equipment, increasing the design pressure rating of the system beyond the requirements of NFPA 58, or providing early detection and isolation of the system to ensure product control. This list is not exhaustive and is not ranked in an order of priority.

Table 9.1
Suggested Alternative Methods for Industrial and Bulk Plants That Do Not Pose a Hazard But Lack a Water Supply

Item #	Possible options to implement when adequate water supply is not available
1	Reduce the service life of hoses.
2	Increase frequency of equipment inspection.
3	Establish a service life program for the maintenance of the container pressure relief devices. This could include the installation of a listed multiple port valve and certifying that the relief devices are properly set and maintained every 5 to 10 years.
4	Increase the design strength of the piping and fitting systems.
5	Install emergency shutoff valves in conjunction with container internal valves.
6	Install emergency shutoff valves downstream of transfer pump outlets and upstream of the vapor and liquid valves at the bulkhead.
7	Install pneumatic tubing along the facility boundary to serve as a perimeter fire detection system. This would provide protection of the facility against exposure fires.
8	Provide optical flame detection or linear heat detection, or a gas detection system connected to an isolation valve installed downstream of every liquid and vapor nozzle on the container. This system could also be monitored to send a signal to an alarm company that notifies the Fire Department of an event.
9	Increase the separation distances of internal facility exposures to the container. These exposures would include a site dumpster, idle or waste pallets and combustibles, and increasing the parking distances between the bobtails and transports in relation to the container.
10	Relocate overhead power lines away from all container and cylinder storage areas to protect against ignition in the event of a line dropping due to wind or power pole impact.
11	Eliminate all combustible vegetation within 30 feet of the LP-Gas container. This can be accomplished using gravel, or paving the site yard.
12	Install tanks using the mounding or burial method.



General Notes

ALL DRAWINGS ARE EXCLUSIVE PROPERTY OF AMERICAS PROPANE AND CANNOT BE REPRODUCED WITHOUT WRITTEN PERMISSION

No.	Revision/Issue	Date

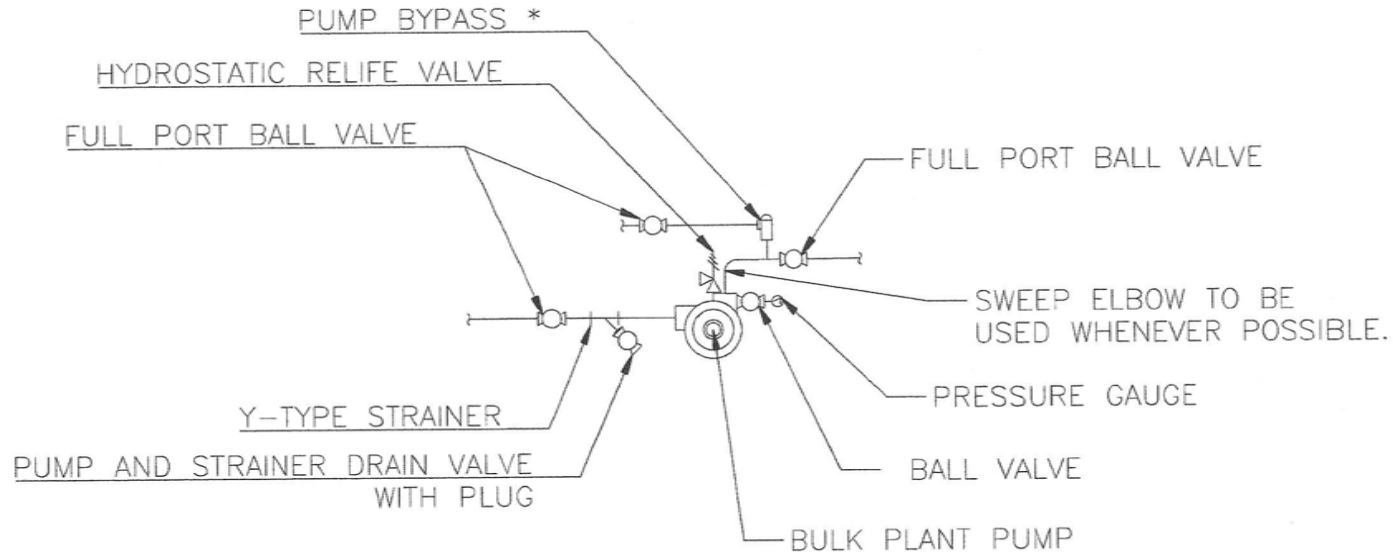
Drawing Name
EDGARTOWN PROPOSED UPGRADE TO 4 30000 GALLON TANKS.

Project Name and Address
Edgartown

Asn	Stamp
Drawing Number	
Author	

CORKEN Z3500 SERIES PREFERRED
 BLACKMER 3LGLD ALTERNATIVE
 MEC HIGH FLOW BYPASS MEBV2 TO BE USED

* PUMP BYPASS TO BE
 PLACED IN PIPING
 AFTER THE ELBOW. NEVER
 ON TEE EXITING PUMP.



General Notes

No.	Revision/Issue	Date

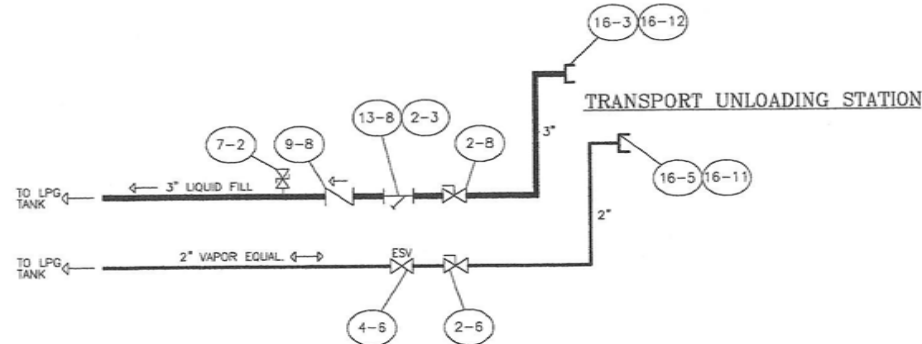
Drawing Name
**BULK PLANT
 PUMP INSTALLATION**

Project Name and Address
**Project 9
 PUMP INSTALLATION**

Area ###	Zone
Drawing Number ###	
Author root	

BILL OF MATERIAL

SYMBOL	QTY.	DESCRIPTION	MATERIAL	PIPE SIZE	MANUFACTURER/PART NO.
2-3	1	BALL VALVE (THREADED)		3/4"	JOWR 300-884
2-6	1	BALL VALVE (THREADED)		2"	JOWR 300-308
2-8	1	BALL VALVE (THREADED)		3"	JOWR 300-310
4-6	1	EMERGENCY VALVE	FNPT/FNPT	2"	MIRSWALL EXCELSDOR M2550-18
7-2	1	WELD RELIEF VALVE	WNPT	1/2"	MIRSWALL EXCELSDOR M2550-180
9-8	1	BACKCHECK VALVE	FNPT/FNPT	3"	MIRSWALL EXCELSDOR M2570-24
13-8	1	STRAINER	FNPT/FNPT	3"	MIRSWALL EXCELSDOR M2580
16-3	1	STEEL COP		3 1/4"	MIRSWALL EXCELSDOR M2400-1
16-5	1	STEEL COP		3 1/4"	MIRSWALL EXCELSDOR M2400-1
16-11	1	ACME ADAPTOR	FLANGE/WNPT	3 3/4"	MIRSWALL EXCELSDOR M2514
16-12	1	ACME ADAPTOR w/ SCREEN	FLANGE/WNPT	3 3/4"	MIRSWALL EXCELSDOR M2528



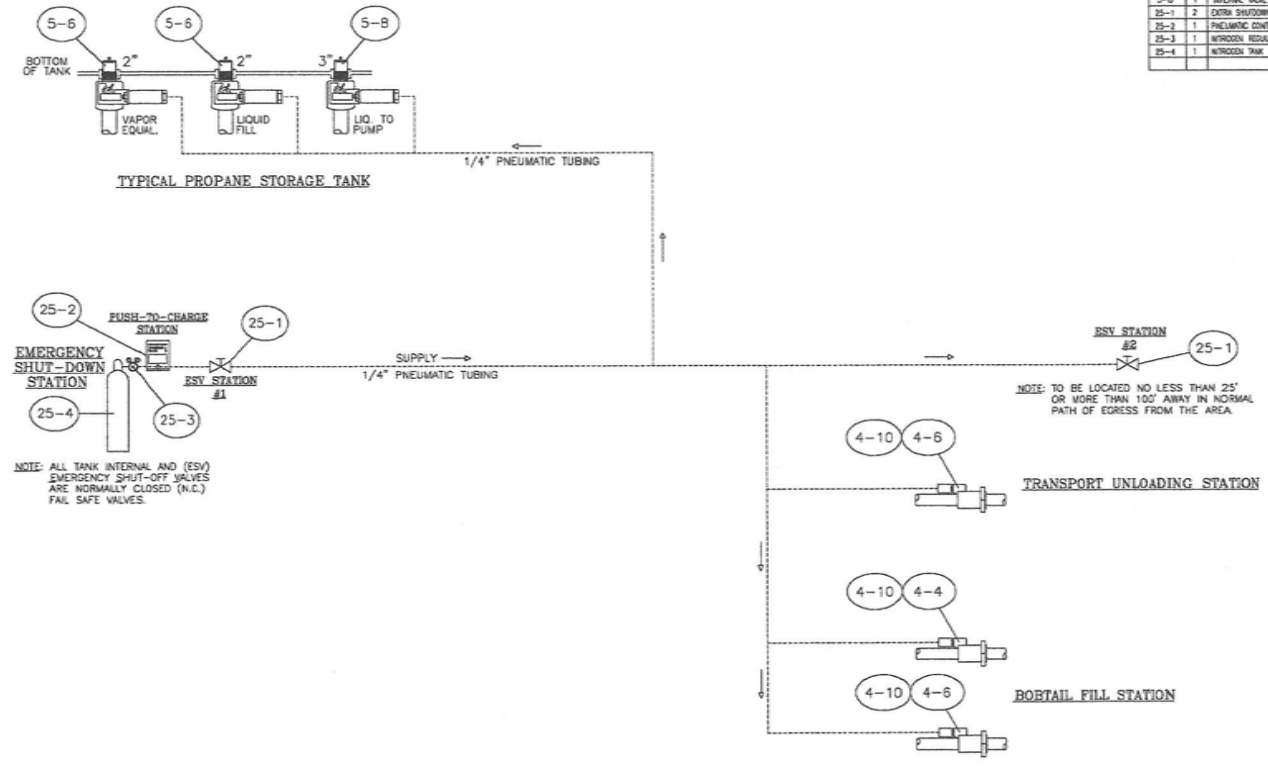
P & I D DIAGRAM
SCALE NONE

GENERAL NOTES:

- 1.) ALL PIPING TO BE ASTM A53 OR ASTM 106 WELDED OR SEAMLESS CARBON STEEL PIPE.
- 2.) ALL TEES, ELBOWS, COUPLINGS, UNIONS, ETC. WILL BE EXTRA HEAVY FORGED STEEL WHEN INSTALLED ON HIGH PRESSURE SERVICE PIPING OPERATING AT GREATER THAN 125 PSIG OR MALLEABLE STEEL WHEN INSTALLED ON (LOW PRESSURE) SERVICE PIPING OPERATING AT LESS THAN 125 PSIG.
- 3.) ALL FLANGES (150 LB. LOW PRESSURE/300 LB. HIGH PRESSURE) SHALL BE DESIGN FOR A PRESSURE RATING EQUAL TO OR GREATER THAN THE REQUIRED WORKING PRESSURE OF THE PIPING SERVICE FOR WHICH THEY ARE INSTALLED.
- 4.) ALL (HIGH PRESSURE) LIQUID AND VAPOR SERVICE PIPING OPERATING AT GREATER THAN 125 PSIG WILL BE SCHEDULE 40 WHEN WELDED AND/OR SCHEDULE 80 WHEN THREADED.
- 5.) ALL (LOW PRESSURE) VAPOR SERVICE PIPING OPERATING AT LESS THAN 125 PSIG WILL BE SCHEDULE 40 WHEN WELDED AND/OR THREADED.

TRANSPORT UNLOADING
P&ID
AMERICAS
KING OF PRUSSIA, PA
 DWG. NO. 1602-015 Sheet 0 of 0

BILL OF MATERIAL				
QTY.	DESCRIPTION	UNIT/OUTLET	PPE SIZE	MANUFACTURER/PART NO.
4-4	1	EMERGENCY VALVE	1 1/4"	MARSHALL EXCELSIOR 4E85-10
4-6	2	EMERGENCY VALVE	2"	MARSHALL EXCELSIOR 4E85-16
4-10	3	PNEUMATIC ACTUATOR	2"	MARSHALL EXCELSIOR 4E85-10
5-6	2	INTERNAL VALVE (250 GPM)	2"	MARSHALL EXCELSIOR 4E85B-16
5-8	1	INTERNAL VALVE (250 GPM)	3"	MARSHALL EXCELSIOR 4E85B-24
25-1	2	ESV SHUTDOWN VALVE		REGD 705994-04
25-2	1	PNEUMATIC CONTROL KIT		REGD 705994-05
25-3	1	NITROGEN REGULATOR		
25-4	1	NITROGEN TANK		



E.S.V. PNEUMATIC CONTROL VALVE FLOW DIAGRAM
SCALE NONE

EMERGENCY SHUTDOWN SYSTEM

A 230 CUBIC FOOT NITROGEN BOTTLE IS USED AS THE SUPPLY SOURCE REQUIRED TO ENERGIZE "HOLD OPEN" ALL EMERGENCY SHUTOFF VALVES (ESV'S) AND INTERNAL VALVES LOCATED THROUGHOUT THE PROPANE SYSTEM. ALL EMERGENCY/INTERNAL SHUTOFF VALVES ARE NORMALLY CLOSED (NC) FAIL SAFE VALVES AND AS SUCH WILL CLOSE AUTOMATICALLY WITH EITHER LOSS OF PNEUMATIC PRESSURE TO THE ACTUATOR CAUSING THEM TO CLOSE UNDER THEIR OWN SPRING TENSION AND/OR UNDER FIRE CONDITIONS WHEN AN INTERNAL DESIGNED FUSIBLE LINK WELTS. 50 PSIG IS THE REQUIRED NITROGEN PRESSURE TO HOLD OPEN ALL EMERGENCY/INTERNAL VALVES.

HOW THE PNEUMATIC (NITROGEN) SHUTDOWN SYSTEM WORKS

TO "CHARGE" THE EMERGENCY SHUTDOWN SYSTEM:
UPON ACTIVATION OF THE "PUSH-TO-CHARGE" BUTTON (PART #25-2) LOCATED AFTER THE NITROGEN BOTTLE REGULATOR A PRE-SET AMOUNT/PRESSURE 50 PSIG NITROGEN FILLS THE 1/4" PNEUMATIC TUBING CAUSING ALL ESV'S AND INTERNAL VALVES TO OPEN.
ONCE THE NITROGEN SUPPLY PRESSURE FROM THE BOTTLE IS NO LONGER NEEDED AND SHUTS OFF ONCE THE "PUSH-TO-CHARGE" BUTTON IS RELEASED AND HAS FILLED THE PNEUMATIC TUBING WITH NITROGEN TO PRESSURE.

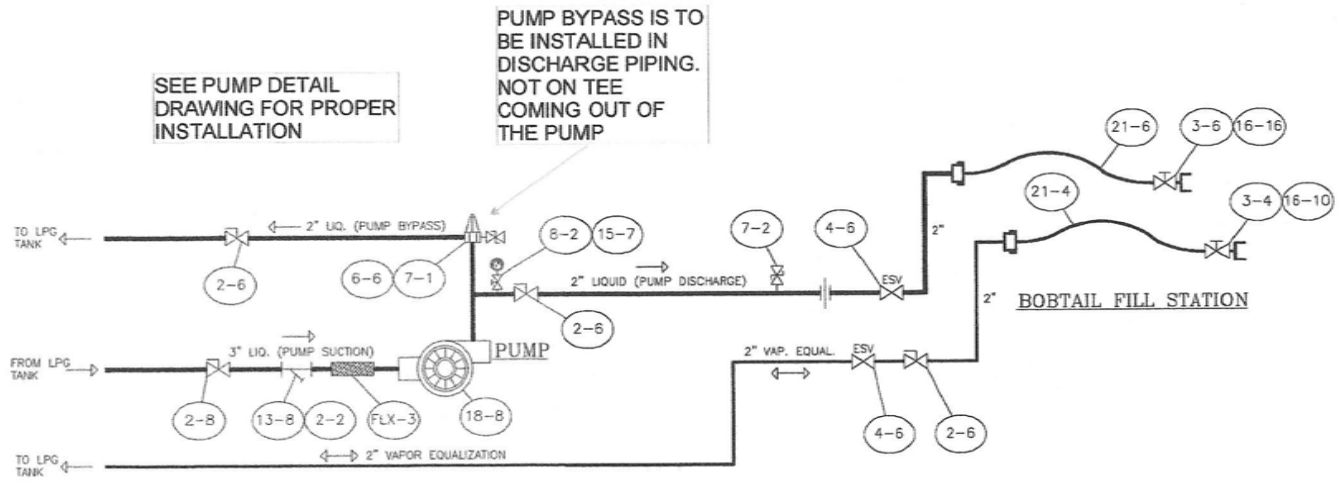
TO "ACTIVATE" ANY ONE OF THE REMOTE EMERGENCY SHUTDOWN STATIONS:
UPON ACTIVATION OF ANY ONE OF THE REMOTE "PUSH-TO-CLOSE" STATIONS (#1) & (#2) THE SET AMOUNT OF NITROGEN PRE-CHARGED INTO THE PNEUMATIC TUBING WILL BE IMMEDIATELY PURGED TO ATMOSPHERE CAUSING ALL CONNECTED EMERGENCY/INTERNAL VALVES TO CLOSE. THE ONLY WAY TO OPEN THESE VALVES AGAIN IS TO PUSH THE "PUSH-TO-CHARGE" (PART #25-2) BUTTON WHICH WILL RELEASE THE PRE-SET AMOUNT/PRESSURE FILLING THE PNEUMATIC TUBING CAUSING THE VALVES TO OPEN. THIS IS A FAIL SAFE EMERGENCY SHUTDOWN AS REQUIRED AND ACCEPTED BY NFPA #58, THE LP GAS CODE.

HILTZ PROPANE SYSTEMS, INC.
893 WEST MARKET STREET
MARIETTA, PENNSYLVANIA 17547
PHONE: (717) 604-1890
HILTZPROPANESYSTEMS.COM

ESV/PNEUMATIC DIAGRAM
AMERICAS
KING OF PRUSSIA, PA
DWG. NO. 1802-015 Sheet 0 of 0

BILL OF MATERIAL

SYMBOL	QTY.	DESCRIPTION	INLET/OUTLET	PIPE SIZE	MANUFACTURER/ PART NO.
2-3	1	BALL VALVE (THREADED)		1"	JOHN 500-305
2-6	2	BALL VALVE (THREADED)		2"	JOHN 500-305
2-8	1	BALL VALVE (THREADED)		3"	JOHN 500-310
3-4	1	GLOBE VALVE (THREADED)		1 1/4"	WARRHALL EXCELSIOR M625-10
3-6	1	GLOBE VALVE (THREADED)		2"	WARRHALL EXCELSIOR M625-16
4-6	1	EMERGENCY VALVE	FMP/FMP	2"	WARRHALL EXCELSIOR M625-16
6-6	1	BRASS VALVE	FMP/FMP	2"	WARRHALL EXCELSIOR M640-8
7-1	2	WDRD. RELIEF VALVE	MPT	1/4"	WARRHALL EXCELSIOR M625-150
7-2	5	WDRD. RELIEF VALVE	MPT	1/2"	WARRHALL EXCELSIOR M625-150
8-2	2	WDRD. VALVE	MPT/FMP	1/4"	WARRHALL EXCELSIOR M625-11
14-8	1	BACKCHECK VALVE	FMP/FMP	3"	WARRHALL EXCELSIOR M625-24
10-8	3	CESS FLOW VALVE	FMP/FMP	2"	WARRHALL EXCELSIOR M625-16
13-8	2	STRAINER	FMP/FMP	3"	WARRHALL EXCELSIOR M625
15-7	1	2 1/4" LG TUBED PN DI (B-HSE)		1/4"	WARRHALL EXCELSIOR M645
15-10	1	TIEER COUPLING		1 3/4" HP	WARRHALL EXCELSIOR M64B-10
15-16	2	TIEER COUPLING		1 1/2" HP	WARRHALL EXCELSIOR M64B-10
18-8	1	RAMP w/ 10 HP MOTOR			CORDEX 23520 w/ 10 HP MOTOR
21-4	1	1 1/4" LPG HOSE	MPT	1 1/4"	
21-6	1	2" LPG HOSE	MPT	2"	
FLX-3	1	3" FLEX CONNECTOR		3"	



SEE PUMP DETAIL DRAWING FOR PROPER INSTALLATION

PUMP BYPASS IS TO BE INSTALLED IN DISCHARGE PIPING. NOT ON TEE COMING OUT OF THE PUMP

P. & I. D. DIAGRAM
SCALE NONE

GENERAL NOTES:

- 1.) ALL PIPING TO BE ASTM A53 OR ASTM 106 WELDED OR SEAMLESS CARBON STEEL PIPE.
- 2.) ALL TEES, ELBOWS, COUPLINGS, UNIONS, ETC. WILL BE EXTRA HEAVY FORGED STEEL WHEN INSTALLED ON (HIGH PRESSURE) SERVICE PIPING OPERATING AT GREATER THAN 125 PSIG OR MALLEABLE STEEL WHEN INSTALLED ON (LOW PRESSURE) SERVICE PIPING OPERATING AT LESS THAN 125 PSIG.
- 3.) ALL FLANGES (150 LB. LOW PRESSURE/300 LB. HIGH PRESSURE) SHALL BE DESIGN FOR A PRESSURE RATING EQUAL TO OR GREATER THAN THE REQUIRED WORKING PRESSURE OF THE PIPING SERVICE FOR WHICH THEY ARE INSTALLED.
- 4.) ALL (HIGH PRESSURE) LIQUID AND VAPOR SERVICE PIPING OPERATING AT GREATER THAN 125 PSIG WILL BE SCHEDULE 40 WHEN WELDED AND/OR SCHEDULE 80 WHEN THREADED.
- 5.) ALL (LOW PRESSURE) VAPOR SERVICE PIPING OPERATING AT LESS THAN 125 PSIG WILL BE SCHEDULE 40 WHEN WELDED AND/OR THREADED.

BOBTAIL FILL P&ID
AMERICAS
KING OF PRUSSIA, PA

DWG. NO. 1802-015 Sheet 0 of 0

DATE: J.P.V. 3/17/18
SCALE: NONE
DRAWN BY: [REDACTED]
CHECKED BY: [REDACTED]
APPROVED BY: [REDACTED]

TANK DATA PLATE

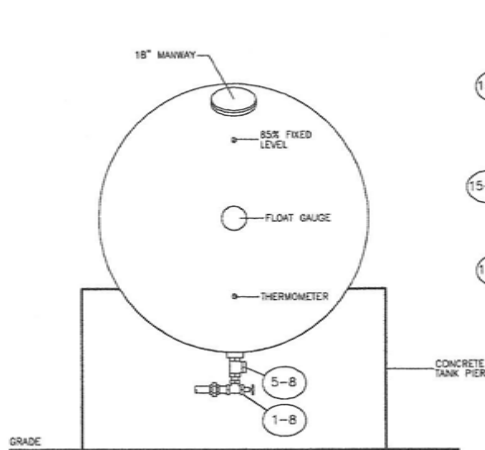
NATIONAL BOARD NO.	T80		
NATIONAL BOARD INSPECTED	250 PSI @ 125° F		
MAXIMUM ALLOWABLE WORKING PRESSURE	[]		
WFR. SR. NO.	T80		
D.S. SURFACE AREA (SQ. FT.)	1,517	HEADS	FEW
WATER GALS.	30,000	WATER LBS.	250,000
131.875"	T80	T80	46'-9 7/8"
DIA.	SHELL THK.	HEAD THK.	GALL.
T80	A/C	T80	
WFR. BY	7PC	YEAR BUILT	

TANK SAFETY RELIEF DATA

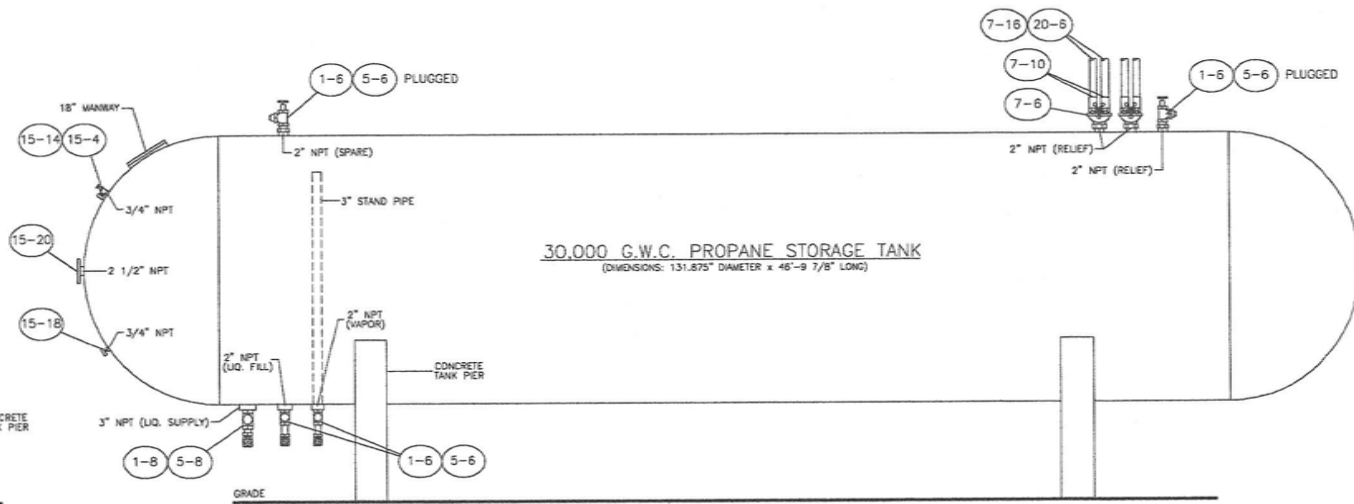
TANK SIZE ASME (G.W.C.)	TANK SURFACE AREA (SQ. FT.)	N.F.P.A. #68 REQ'D. RELIEF CAPACITY (S.C.F.M.)	RELIEF VALVE CAPACITIES
			MARSHALL EXCELSIOR (NO.) - (S.C.F.M.)
30,000	1,688	25,180	#MEV125/250 - 6,328 (8)

BILL OF MATERIAL

SYMBOL	QTY.	DESCRIPTION	INLET/OUTLET	PIPE SIZE	MANUFACTURER/ PART NO.
1-8	4	ANGLE VALVE (THREADED)	FNPT/FNPT	2"	MARSHALL EXCELSIOR ME15-16
1-8	1	ANGLE VALVE (THREADED)	FNPT/FNPT	3"	MARSHALL EXCELSIOR ME15-24
5-8	4	INTERNAL VALVE (THREADED)	MNPT/FNPT	2"	MARSHALL EXCELSIOR ME990R-16
5-8	1	INTERNAL VALVE (THREADED)	MNPT/FNPT	3"	MARSHALL EXCELSIOR ME990R-24
7-8	2	RELIEF VALVE (12,481 SCFM)	MNPT	2"	MARSHALL EXCELSIOR ME945-168/250
7-10	8	RELIEF VALVE (6,328 SCFM)	MNPT	1 1/4"	MARSHALL EXCELSIOR ME125/250
7-16	8	GALVANIZED STACK		2"	2"x7'-0" SCHEDULE 40
15-4	1	1/2" PRESSURE GAUGE (0-300#)	MNPT	1/4"	MARSHALL EXCELSIOR ME1580
15-14	1	VENT/PRESSURE GAUGE	MNPT	3/4"	MARSHALL EXCELSIOR ME1450
15-18	1	THERMOMETER		1/2"	MARSHALL EXCELSIOR ME1701
15-20	1	LIQUID LEVEL FLOAT GAUGE		2 1/2"	MARSHALL EXCELSIOR ME940-108
20-8	8	METAL RAIN CAP		2"	



HEAD-END ELEVATION DETAIL
SCALE: NONE



SIDE ELEVATION DETAIL
SCALE: NONE

30,000 GWC TANK TRIM DETAIL
131" DIAMETER
AMERIGAS
KING OF PRUSSIA, PENNSYLVANIA
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